

A retrofitted activated-sludge plant with sequential nitrification and anammox obtains dischargeable effluent

Joop Colsen¹, Joachim Desloover², Haydée De Clippeleir², Pascal Boeckx³, Gijs Du Laing⁴,
Willy Verstraete² (presenter), Siegfried E. Vlaeminck²



¹ Environment and energy Colsen International B.V. (E-mail: j.colsen@colsen.nl)

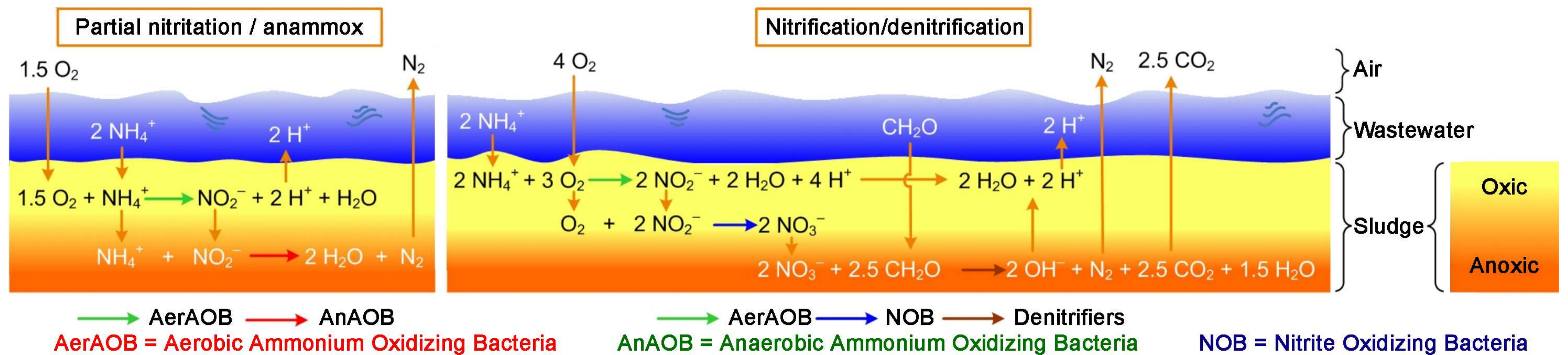
² Laboratory of Microbial Ecology and Technology (LabMET), Ghent University, (E-mail: Siegfried.Vlaeminck@UGent.be)

³ Laboratory of Applied Physical Chemistry (ISOFYS), Ghent University

⁴ Laboratory of Analytical Chemistry and Applied Ecochemistry (EcoChem), Ghent University

- Introduction:**
- New Activated Sludge (NAS[®]) represents a hybrid, floc-based nitrogen removal process
 - process is based on solids control, retention times (SRT) and dissolved oxygen (DO) levels
 - full-scale NAS[®] plant is examined (treating anaerobically digested industrial wastewater)
 - serial anammox, denitrification and nitrification compartments are followed by a final settler
 - in the anammox step 77% of the nitrogen is removed
 - **overall nitrogen removal efficiency = 95% yielding a dischargeable effluent**

Figure 1: Comparative representation of the catabolic reactions of the partial nitrification / anammox and the nitrification/de-nitrification steps



Experimental approach:

- test location : full scale WWTP of a potato-processing plant
- N-removal plant was previously operated in conventional activated-sludge mode
- the system is retrofitted to a hybrid nitrogen removal process
- step 1 : anaerobic digestion and struvite precipitation (Anphos[®])
- step 2 : nitrification/denitrification system
- full-scale nitrogen removal process discharges effluent to surface water
- WWTP control via DO setpoints and SRT



Figure 2: Aerial view of WWTP at LWM, Bergen op Zoom (The Netherlands)

Results and discussion:

Table 1: Water and nitrogen streams for partial nitrification, anammox, denitrification and nitrification reactors (averages ± standard deviations)

Partial Nitrification & Anammox				Denitrification			Nitrification			Stream
PN	RET	REC1	AN	AN	REC2	DN	DN	REC2	OUT	
2366	4080	36	6410	5601	4800	10401	10997	4800	6197	Q (m ³ d ⁻¹)
203±15	0.0±0.0	0.3±0.0	55±1	0.0±0.0	0.0±0.0	0.0±0.0	74±3	0.0±0.0	0.0±0.0	NH ₄ ⁺ (kg N d ⁻¹)
266±9	1.0±1.0	0.3±0.0	52±3	89±9	0.0±0.0	27±3	1.0±0.0	0.0±0.0	0.0±0.0	NO ₂ ⁻ (kg N d ⁻¹)
79±8	10±3	0.1±0.0	21±4	20±4	24±2	13±3	27±1	45±3	58±4	NO ₃ ⁻ (kg N d ⁻¹)

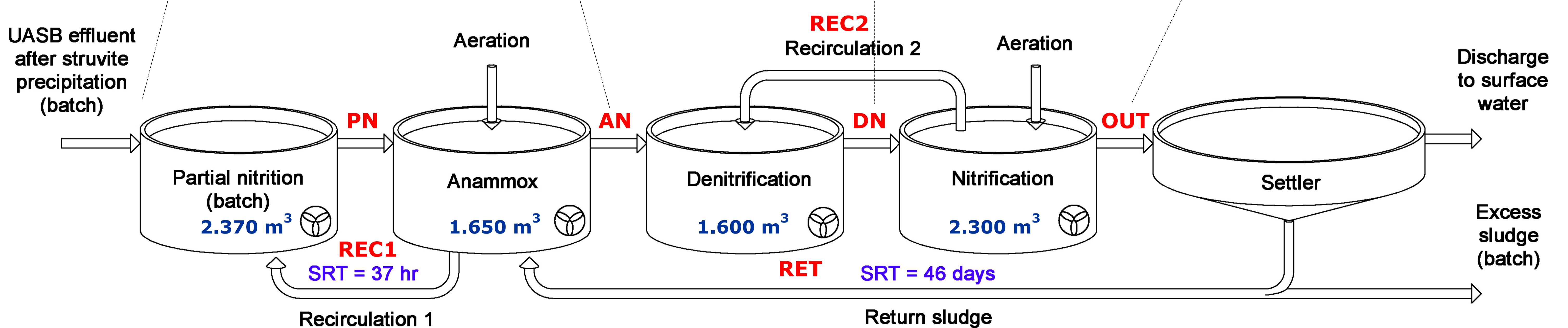


Figure 3: Schematic overview of the examined WWTP hybrid nitrogen removal process

Conclusions:

- An existing WWTP was successfully retrofitted to obtain a New Activated Sludge (NAS[®]) floc based N-removal process.
- The retrofit project of the Nitrification/Denitrification plant to new NAS[®] floc based process resulted in 30% less energy consumption & 50% less sludge production.
- N-oxidation (nitrification) of the residual N results in the formation of NO₂⁻ (45-47%) & NO₃⁻ (13-15 %).
- In the anammox stage ~77% of all Nitrogen is converted. The biomass in the anammox stage consists for 3 % out of *Kuenenia* species, while they are responsible for the conversion of 70% of the Nitrogen.
- The overall nitrogen removal efficiency over all steps = 95%.
- Dischargeable effluent is obtained with Nitrogen concentration < 10 mg N x L⁻¹.
- More efficient WWTP's can now be designed, which will allow the construction of more compact installations with higher loading rates.

Acknowledgements:

J.D. and H.D.C. are recipients of a PhD grant from the Institute for the Promotion of Innovation by Science and Technology in Flanders (IWT-Vlaanderen, numbers SB-091144 and SB-81068) and S.E.V. was supported as a postdoctoral fellow from the Research Foundation Flanders (FWO-Vlaanderen). The authors gratefully thank Senternovem for the financial support through the 'Innovator' programme (DWZ0644224, project number IWA06012).